



Quick Reference Card

Typical Condensate Return System Optimizations

Problem	Potential Cause	Optimizations
Stalled Heat Exchanger (due to insufficient pressure differential across the steam trap)	High back pressure due to: <ul style="list-style-type: none"> • Pipe elevations • Undersized pipes • Blowing steam traps • Addition of new condensate return flows to the same pipe 	<ul style="list-style-type: none"> • Reduce or eliminate back pressure • Use good piping and design practices (Size and install heat exchangers, piping, and valves properly) • Use good maintenance practices (clean strainers before control valve and steam trap) • Install an Armstrong Double Duty steam trap or pumping trap • Install a safety drain trap and vacuum breaker • Install an Armstrong Posi-Pressure system • Install an open receiver and condensate pump • Clean strainers before control valve and steam trap in order to eliminate restricted flow and excessive pressure drop
	Reduced inlet pressure due to: <ul style="list-style-type: none"> • Modulating steam supply • Plugged strainer • Decrease in steam supply pressure • Oversized Equipment 	
Water Hammer Pressure differential in the system caused by: <ul style="list-style-type: none"> • Hydraulic shock • Thermal shock • Differential Shock 	An incorrect trap: <ul style="list-style-type: none"> • Thermostatic traps, orifice traps, etc. piped onto heat exchangers 	<ul style="list-style-type: none"> • Use correct trap for application
	<ul style="list-style-type: none"> • Sudden valve closing or change of direction 	<ul style="list-style-type: none"> • Close valve more slowly • Substitute silent or non-slam check valves for swing checks, • Install shock arrestors
Condensate Contamination	<ul style="list-style-type: none"> • Bi-phase flow transportation • Mixing cold and hot condensate and/or steam 	<ul style="list-style-type: none"> • Return separately pumped condensate (cold) and steam trap (hot) condensate • Return separately low pressure (LP) (cold) and high pressure (HP) (hot) condensate • Install purge pipes or mixing thermal siphon (MTS) on drip traps • Install flash tanks or open receivers • Repair blowing or plugged traps
	<ul style="list-style-type: none"> • Intalled heat exchanger • Water hammer • Improper start-up and operating procedures (not enough time for warm-up) • Contaminated by cooling water, chilled water or glycol when using the same heat exchanger, coil, or jacketed vessel • Boiler water and steam quality issues 	
Flash Steam Venting	<ul style="list-style-type: none"> • High pressure condensate discharge to open receiver 	<ul style="list-style-type: none"> • Eliminate the root cause for contamination: • See solutions for stall and water hammer • Repair leaking pipes in heat exchanger • Repair pump seals • Manage contaminated condensate: • Install Polisher (treat the contamination) • Use as hot water • Recover the heat and then drain condensate to sewer
	<ul style="list-style-type: none"> • Blowing steam traps 	
		<ul style="list-style-type: none"> • Repair/replace steam traps

Quick Reference Card

Typical Condensate Return System Optimizations

Best Practices Piping

- Remove condensate downstream of heat exchanger to prevent stalling, keep tube bundles dry, and reduce corrosion.
- Size piping and valves properly.
- Ensure slow closure of valves.
- Install spring-loaded, center-guided, non-slam, or silent check valves that close before flow reversal.
- Use water hammer arrestors.
- Re-design or re-pipe the system to return hot and cold condensates separately.
- If hot flashing condensate must be discharged into a cool condensate line, it should be discharged through a mixing thermal siphon (MTS), or through a purge pipe in the direction of condensate flow and away from the pipe wall.
- Install flash tanks or open receivers.
- Always have separate lines for dry-closed and pumped condensate return systems. Avoid mixed-condensate systems.
- In installations with high- and low-pressure systems, have two separate dry-closed return lines.
- Avoid lifting condensate lines.
- Add horizontal expansion loops when possible. Try to avoid going up or down. If there is an elevation in condensate line, this is a likely area for erosion.
- Use downward slopes which are critical in keeping condensate lines clear—and also helps prevent corrosion and water hammer.
- All condensate lines should be with a correct slope in direction of the boiler house. Per ASME 31.1 and 31.3, lines that contain a steam/water mix, or require draining periodically, should be pitched downward approx. ¼ inch per foot in the direction of flow.
- Insulate all lines. Armstrong uses the 3E Plus insulation thickness computer program to calculate pipe radiation losses. This program is available as a free download from the links menu and can be used in either I.P. or S.I. units.
- Maximize the size of the header for highest possible flash rate and acceptable velocities (recommended 3000 fpm (15 m/s), not to exceed 5000 fpm (25 m/s)).
- Minimize the length of lines to traps, and long vertical drops to the traps must be back-vented.
- Install proper drip leg ahead of control valves to prevent differential shock from occurring when the control valve is opened after a period of closure.
- Add sample points throughout the condensate system to quickly access condensate for testing.
- Add piping to isolate and safely divert the contaminant when needed.

Armstrong provides intelligent system solutions that improve utility performance, lower energy consumption, and reduce environmental emissions while providing an “enjoyable experience.”



Armstrong International
816 Maple Street, Three Rivers, MI 49093 – USA Phone: (269) 273-1415 Fax: (269) 278-6555
armstronginternational.com